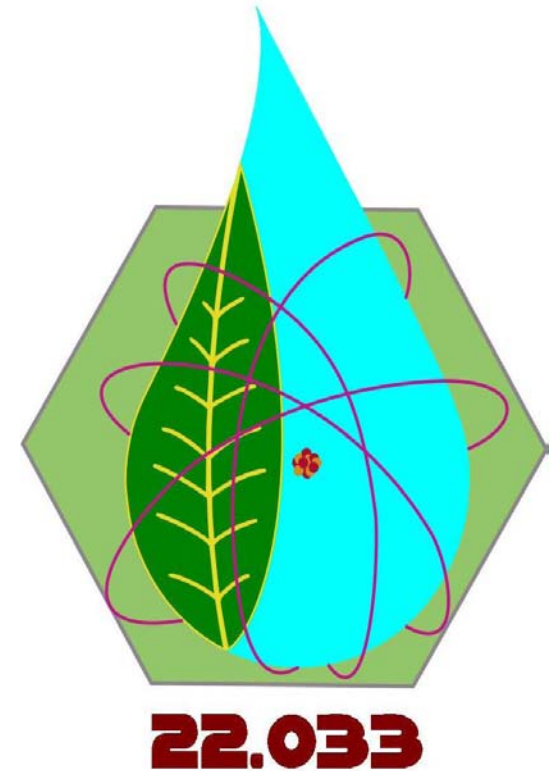


22.033 Process Heat

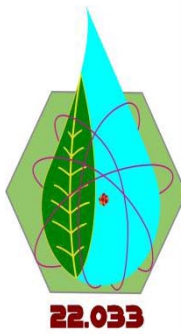
Lauren Ayers
Sarah Laderman
Aditi Verma
Anonymous student



Presentation 1
October 5, 2011

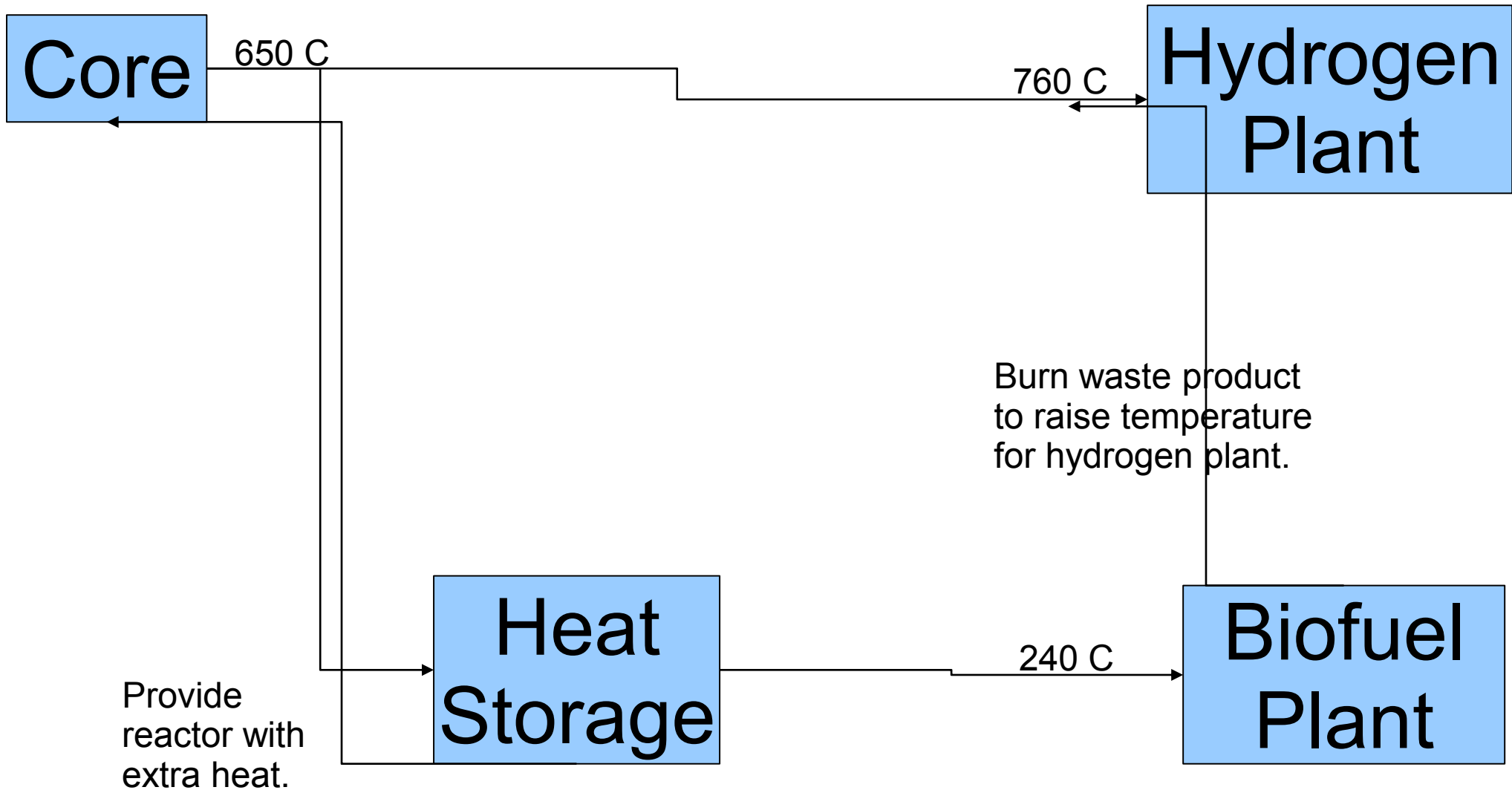


Outline

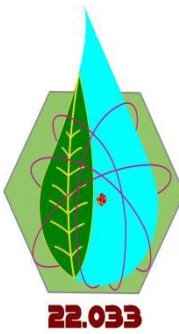


- System Layout
- Heat Exchanger Designs
- Heat Storage Options
- Heat Transport
- Future Work

System Layout

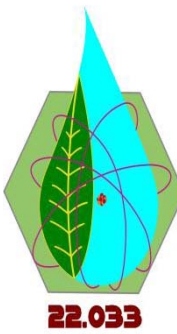


Types of Heat Exchangers Investigated



- Standard shell and tube
- Printed circuit heat exchangers
- Helical shell and tube
- Thermosyphons

Criteria for Selecting a Heat Exchanger



- Operating temperature and pressure
- High heat transfer performance
- Effectiveness
- Fouling



Courtesy of MERUS GmbH. Used with permission.

Multiple Pass Shell and Tube with Continuous Helical Baffles

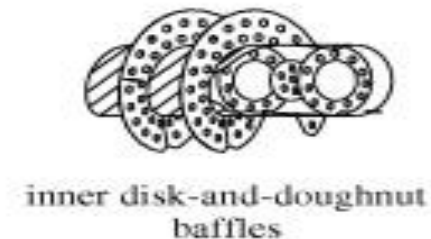
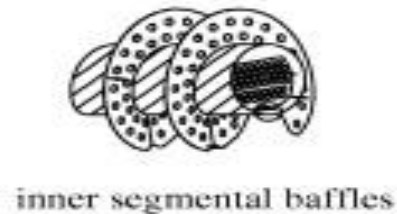
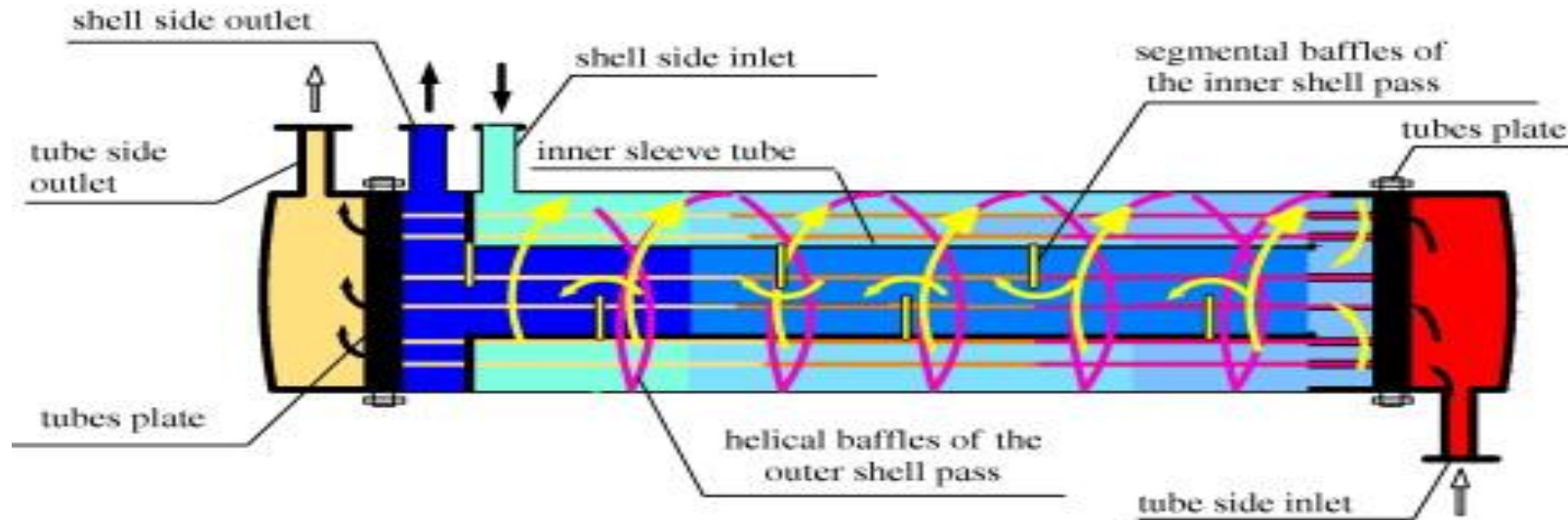
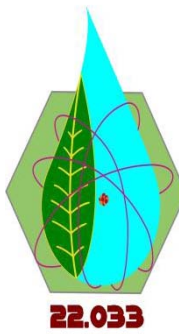


Photo from Q. Wang

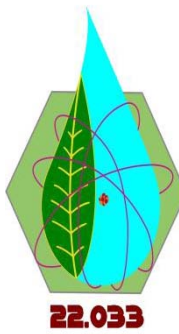
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Max. operating pressure: ~ 70 MPa

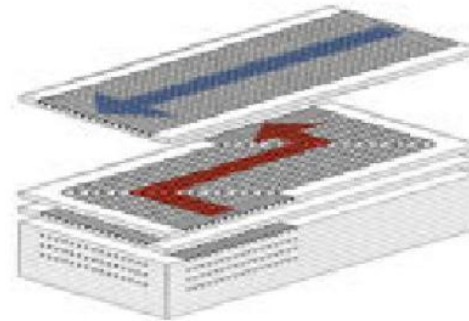
Max. operating temperature: dependent on materials

Induced turbulence + high shear stress = less fouling

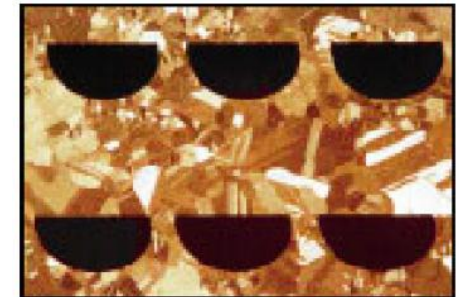
Printed Circuit Heat Exchangers (PCHEs)



- All-metal HXs made of diffusion bonded plates
- Long design life (up to 60 years)
- Compact, mass/duty ratio of 0.2 tons/MW
- High operating temperatures (up to 900 C) and pressure (60 MPa)
- High surface area density (2500 m²/m³)
- Hybrid fin and plate type PCHE, H2X, suitable for coupling gaseous and liquid working fluids

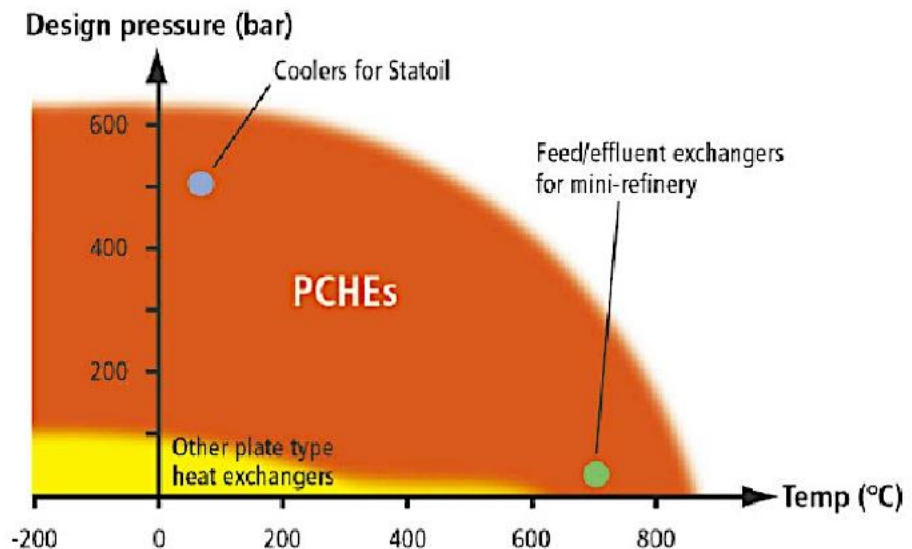


Diffusion bonding of PCHE plates (Heatric™)



Cross sectional view of the semi-circular passages (Heatric™)

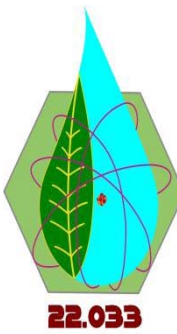
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Current operating experience of Heatric™ PCHEs

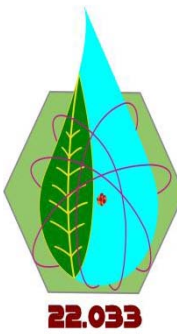
(Gezelius, K., "Design of Compact Intermediate Heat Exchangers for Gas Cooled Fast Reactors," Bachelors' & Masters' Thesis, MIT, June 2004.)

Heat Exchanger Requirements



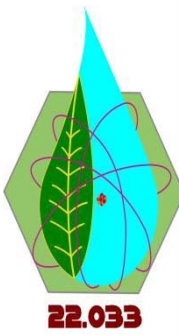
- Operating Temperatures
 - HX connected to CO₂ loop: 650-900 °C
 - Hydrogen plant: 700-900 °C
 - Biofuels plant: 240-300 °C
 - Heat storage: 300-500 °C
- Standardized heat exchanger design will reduce plant complexity and operating and maintenance costs

Heat Exchanger Configurations



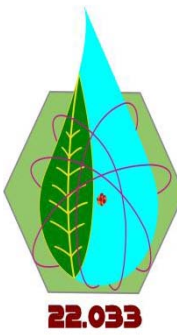
- Two HX instead of single high temperature HX to increase design life
- Connect process heat system in parallel or series
- Remove heat from the secondary cycle before the power conversion system
 - Need to decide with core
- HX decisions will depend on flow rates and temperatures provided by core and needed by biofuels and hydrogen plants

Benefits of Heat Storage



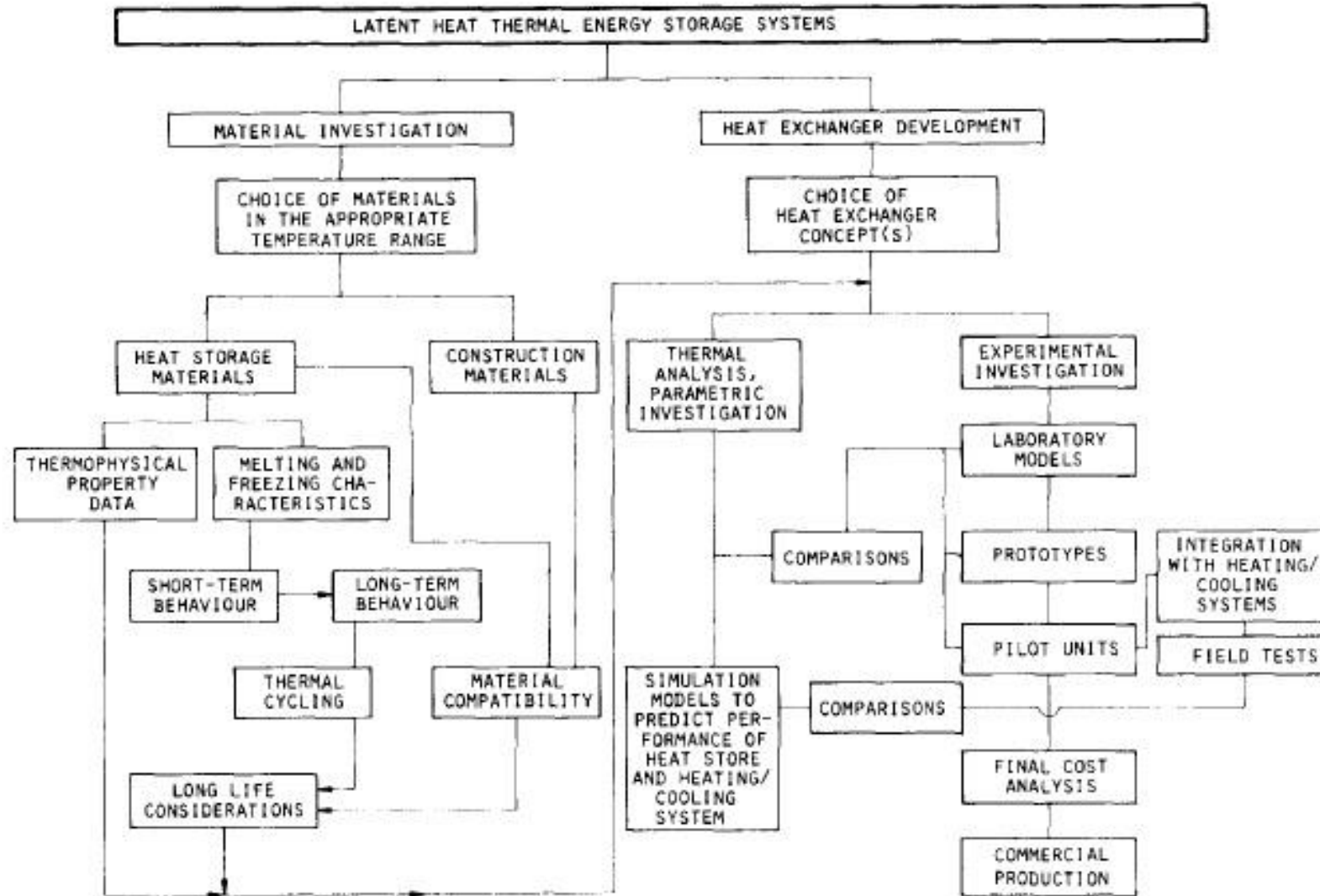
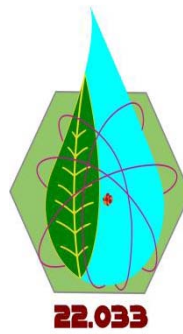
- Plateau energy fluctuations during daily cycles
- Providing lower temperature to biofuels without wasting heat

Heat Storage Options



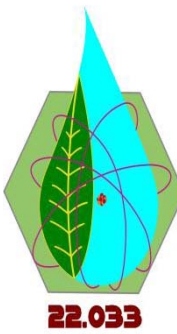
- Latent Heat vs. Sensible Heat
 - Latent – storing energy in chemical bonds
 - Sensible – using change of temperature of material to store heat (specific heat capacity)
- Decided on latent heat
 - Can store higher energy density
 - Provides heat at constant operating temperature
 - Uses phase change materials

Phase Change Material Decision Tree



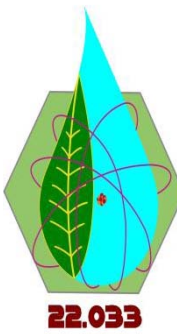
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PCM Selection



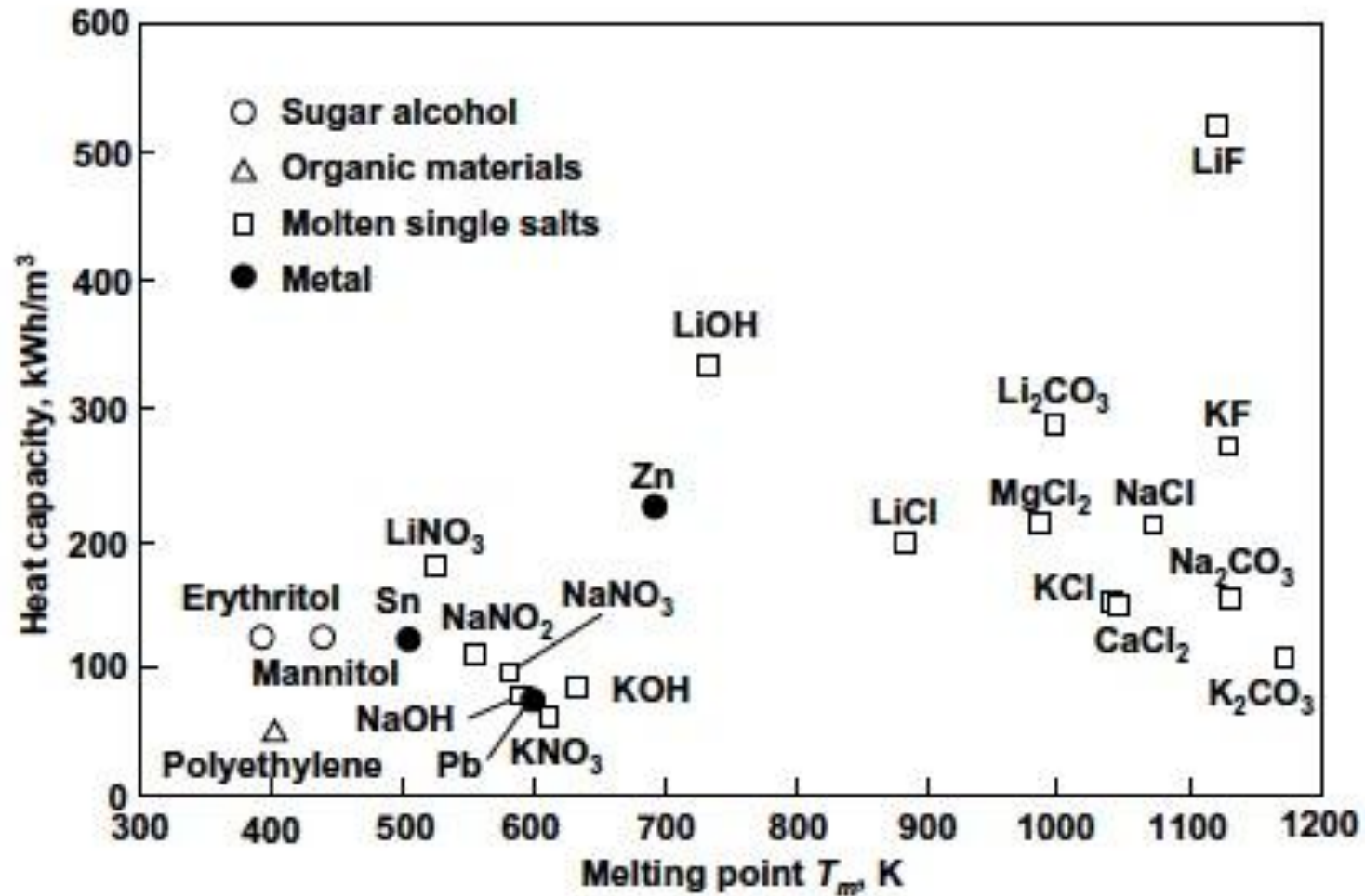
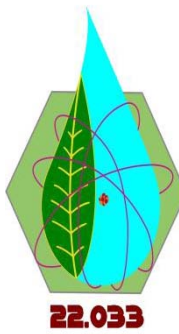
- Must have melting point in desired operating temperature range
- Ideal Characteristics:
 - High latent heat of fusion per unit mass
 - High density
 - High specific heat
 - High thermal conductivity
 - Chemically stable
 - Non-corrosive to the containment material

Liquid-Solid PCMs



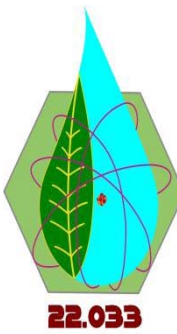
- Paraffins & Salt Hydrates
 - Operating temperature too low
- Salts
 - Large range of operating temperatures
 - Issues: corrosion & low thermal conductivity
- Metals
 - Desirable thermodynamic properties
 - Issues: freezing can cause stresses to containment, temperature range is limited

Salt and Metal PCMs



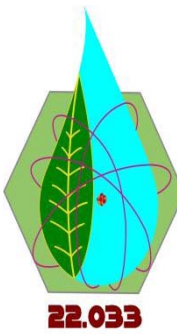
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Looking Ahead



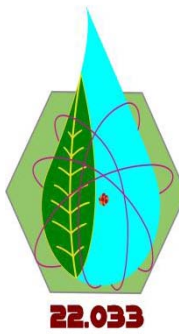
- Containment structure cannot be designed until a PCM is chosen
 - Material compatibility concerns
- Volume of material is dependent on:
 - Thermodynamic properties of the material
 - Amount of energy that needs to be stored

Heat Transport Methods



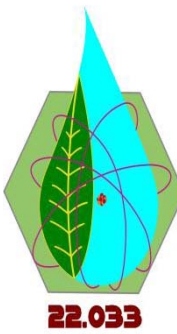
- Thermosyphons
 - Uses gravity and phase changes to move heat long distances with minimal heat loss
 - Highly dependent on location of plant
- Heat pipes
 - Can use capillary action and if in correct orientation, gravity can assist
 - Can also use centripetal, electrokinetic, magnetic, and osmotic forces
 - Not as practical for long distances and not as well developed technologies

Heat Transport Decisions



- Method of condensate transport determined by distance between plants
 - Will model hydrogen plant explosions and biofuel plant fires to determine safe distances
- Material and working fluid determined by HX choice and temperature environment

Future Work



- Finalize heat exchanger and heat storage designs
- Model system once initial outputs/inputs are available
 - Matlab, EES, RELAP
- Heat sink as a safety measure at hydrogen plant
- Determine plant distances as more data becomes available

Questions?

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22.033 / 22.33 Nuclear Systems Design Project
Fall 2011

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