

3.044 MATERIALS PROCESSING

LECTURE 15

Pilkington Sheet Glass Process

Pour molten glass on a liquid, let it settle/flatten and then let it cool

- higher ρ than glass $\rightarrow \rho_{\text{glass}} = 2500 \frac{\text{kg}}{\text{m}^3}$
- liquid temperature \rightarrow between $T_{\text{rigid}} \sim 550^\circ\text{C}$ and $T_{\text{working}} \sim 900^\circ\text{C}$
- immiscible

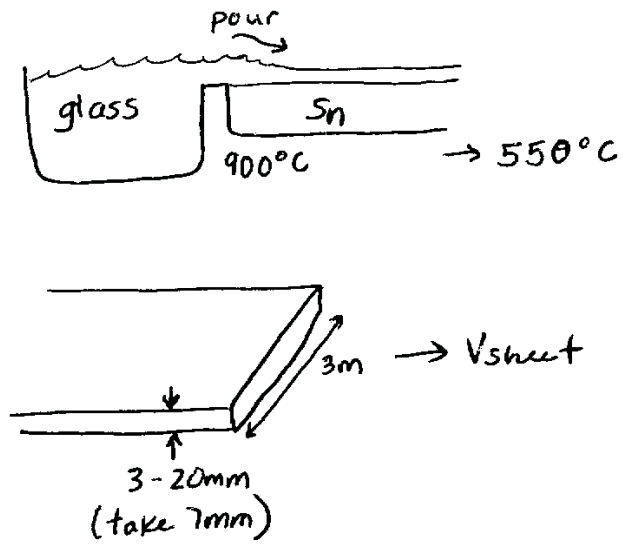
Answer: Liquid Metal

$$\text{Sn (tin)} \rightarrow \rho_{\text{Sn}} = 7000 \frac{\text{kg}}{\text{m}^3}$$

The velocity of the sheet is determined by economic input:

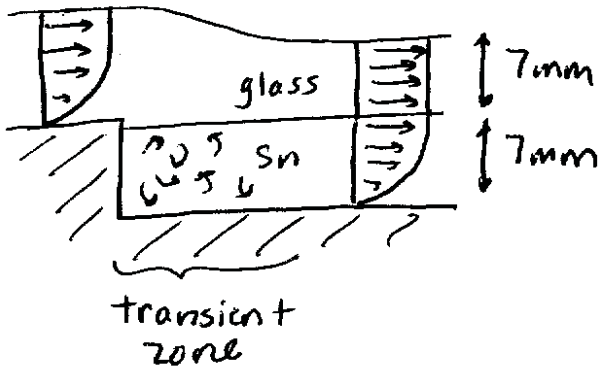
\Rightarrow need 750 tonnes/day to compete with block casting and grinding

$$V_{\text{sheet}} = 10 \frac{\text{m}}{\text{min}}$$



Two Physical Goals

- 1) Fluid Flow → flat, stable film, level glass
- 2) Heat Transfer → cool to 550°C from 900°C



Fluid Flow:

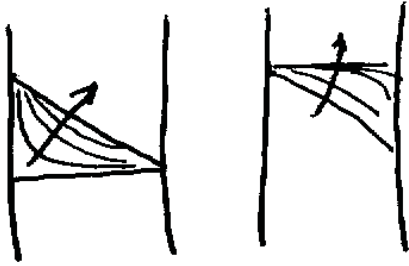
$$\rho_{\text{glass}} = 2500 \frac{\text{kg}}{\text{m}^3}$$

$$\mu_{\text{glass}} = 10^2 \text{ Pa} \cdot \text{s}$$

$$\rho_{\text{Sn}} = 7000 \frac{\text{kg}}{\text{m}^3}$$

$$\mu_{\text{Sn}} = 3 \times 10^{-3} \text{ Pa} \cdot \text{s}$$

How long does it take to remove the transient? How long does it take to get to steady-state?



In Diffusion:

$$\underbrace{\tau}_{\substack{\text{dimensionless} \\ \text{time}}} = \frac{\alpha t}{L^2} = 1$$

$$\tau = \frac{\overbrace{\nu}^{\substack{\text{kinematic} \\ \text{viscosity}}} t}{L^2}$$

$$t_{ss} = \frac{L^2}{\left(\frac{\mu}{\rho}\right)}$$

For glass:

$$L = 0.007 \text{ m}, \quad \mu = 10^2 \text{ Pa} \cdot \text{s}, \quad \rho = 2500 \frac{\text{kg}}{\text{m}^3}$$

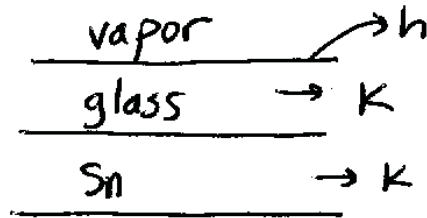
$$\Rightarrow t_{ss} = 0.0001 \text{ s}$$

For tin:

$$L = 0.007 \text{ m}, \quad \mu = 3 \times 10^{-3} \text{ Pa} \cdot \text{s}, \quad \rho = 7000 \frac{\text{kg}}{\text{m}^3}$$

$$\Rightarrow t_{ss} = 114 \text{ s}, \quad V_{\text{sheet}} = 10 \frac{\text{m}}{\text{min}}$$

Length of travel to achieve steady state: $\approx 20 \text{ m}$



Heat Transfer:

Vapor/glass interface: $h = 10 \frac{\text{W}}{\text{m}^2\text{K}}$

Glass: $k = 1.7 \frac{\text{W}}{\text{mK}}$, $L = 0.007 \text{ m}$

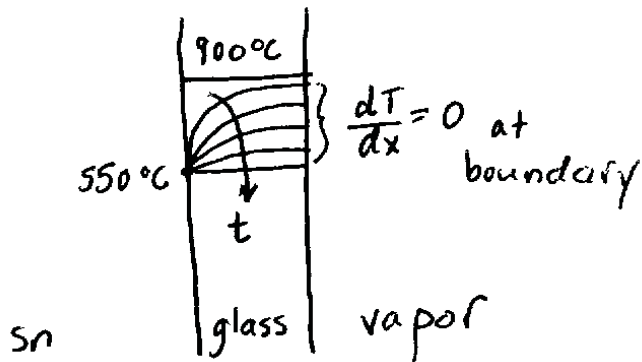
Bi: $\frac{hL}{k} = 0.04$

Bi is **Low!** conduction is **rapid** in glass and convection is **slow**

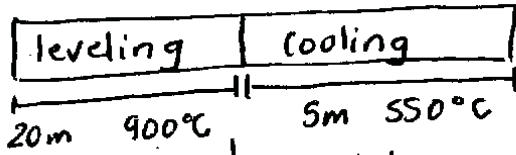
Tin: $k = 35 \frac{\text{W}}{\text{mK}}$

Compare the resistances of glass and Sn:
resistance of Sn is low \rightarrow Sn is a great heat sink

How long does it take to cool?



$\tau = 1$
 $t \approx 15 - 30 \text{ sec}$



↳ can't have a step function of T from 900°C to 550°C so length must increase

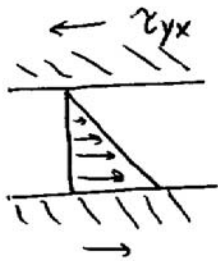
Summary of Fluid Flow

$$\frac{\partial \bar{v}}{\partial t} = \nu \nabla^2 \bar{v} + \frac{\bar{F}}{\rho} - \frac{\nabla P}{\rho}$$

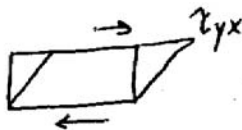
$$\frac{\partial v_x}{\partial t} = \nu \frac{\partial^2 v_x}{\partial y^2} + \frac{F_x}{\rho} - \frac{1}{\rho} \frac{\partial P}{\partial x}$$

Navier-Stokes Equation: solve this with boundary conditions → laminar flow

Fluids can transfer momentum to solids



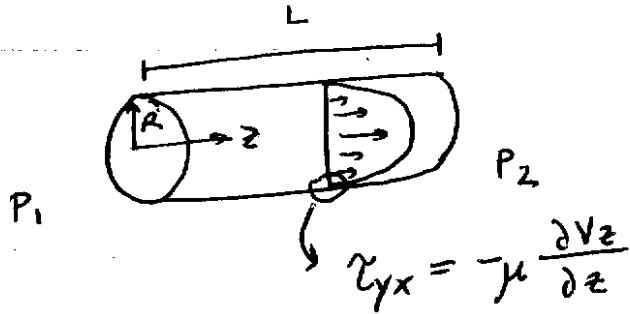
Fluid Flow: $\tau_{yx} = -\eta \frac{\partial v_x}{\partial y}$
 ← is ⊕ stress



Solid Mechanics: $\tau_{yx} = \frac{F}{A}$
 ← is ⊕ stress

} opposite sign convention

Fluid Flow in a Pipe:



Pipe:

$$V_x = \frac{\Delta P}{4L\mu} (R^2 - r^2)$$

At the wall:

$$\tau_{yx} = -\mu \left. \frac{\partial v_z}{\partial r} \right|_{r=R}$$

Stress on the Inner Pipe Wall:

$$\tau_0 = \frac{\mu \Delta P}{4L\mu} 2R = \frac{\Delta P \cdot R}{2L}$$

Kinetic Force: (drag force, total force exerted by the fluid on the solid)

$$\begin{aligned} F_k &= \int_A \tau dA \\ &= \frac{\Delta P R}{2L} 2\pi R L \end{aligned}$$

$$\boxed{F_k = \Delta P \pi R^2}$$

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